

2018 Multi-States Salinity Summit

A Novel Approach for Concentrate Minimization: Phase II



February 8, 2018

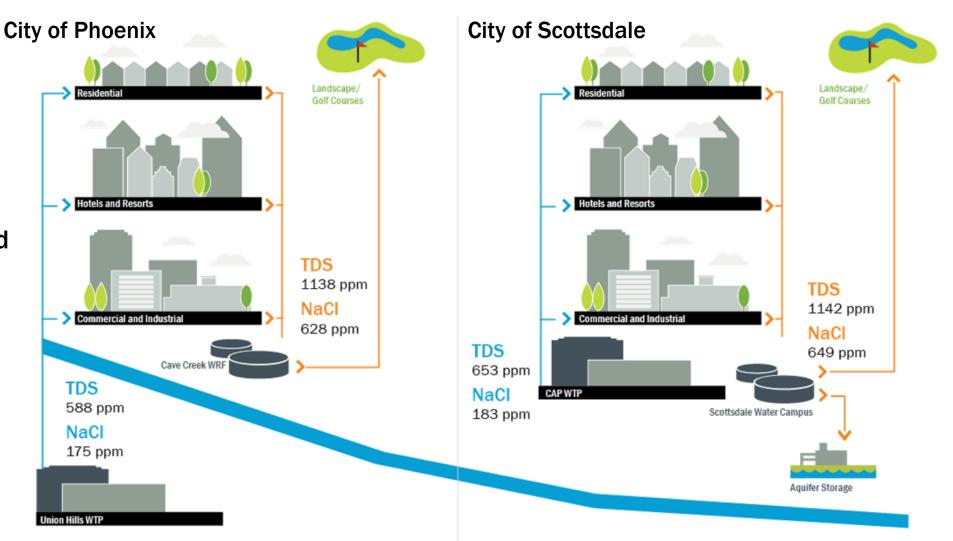






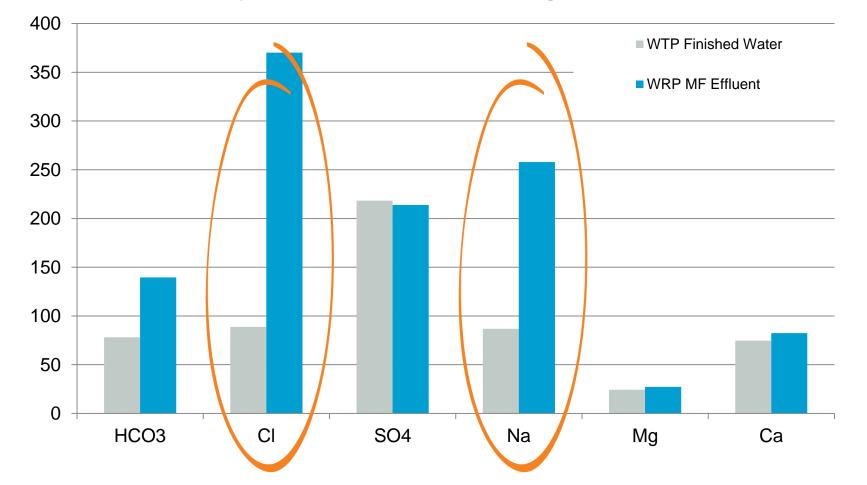
With Hard Waters, More Water Softeners, More Water Quality Impacts

Many utilities' ability to reclaim or discharge treated wastewater is being adversely impacted by elevated sodium and chloride levels.



Comparison of Potable and Reclaimed Water

Major Anions and Cations (mg/L)



NF Membrane Selection

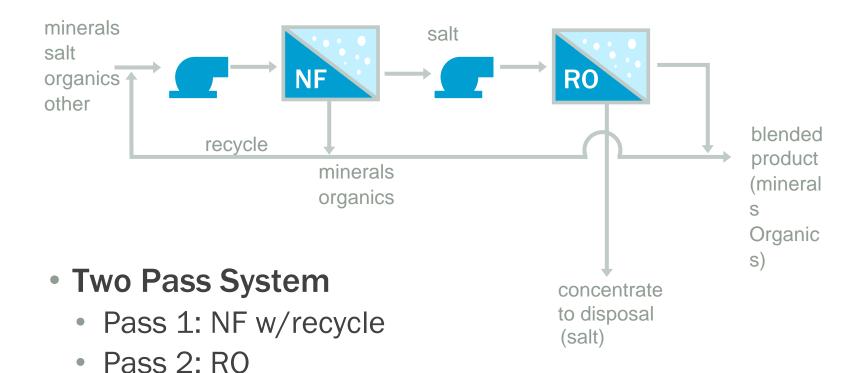
Short duration test of 4 NF products to select one for pilot test

| DOW | CSM | Hydranautics | KMS |
|--------------|------------------------------|---|---|
| 88.5% 64% | 90.9% 54% | 87.0% 60.3% | 82.1% 26.2% |
| 45% | 41% | 46% | 38% |
| 79.2% | 81.5% | 79.1% | 83.2% |
| 92.7% | 93.0% | 93.3% | 93.7% |
| | 88.5% 64% 45% 79.2% | 88.5% 90.9% 64% 54% 45% 41% 79.2% 81.5% | 88.5% 90.9% 87.0% 64% 54% 60.3% 45% 41% 46% 79.2% 81.5% 79.1% |



NF Membrane Test

Pilot Study Schematic



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len-Bradley

Scalable system: 30 gpm

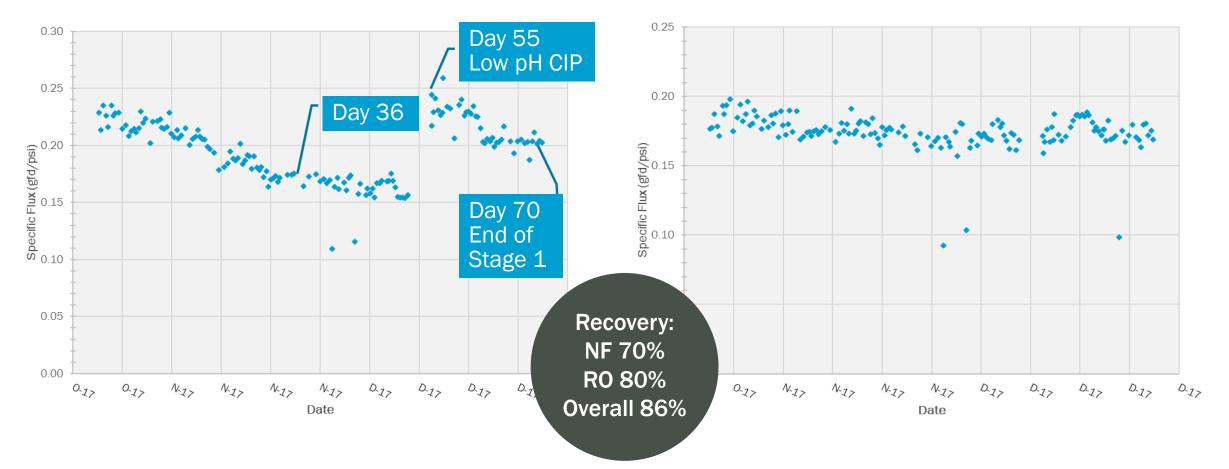
Match RO Recovery, Minimize Chemical Addition

Stage 1 Test



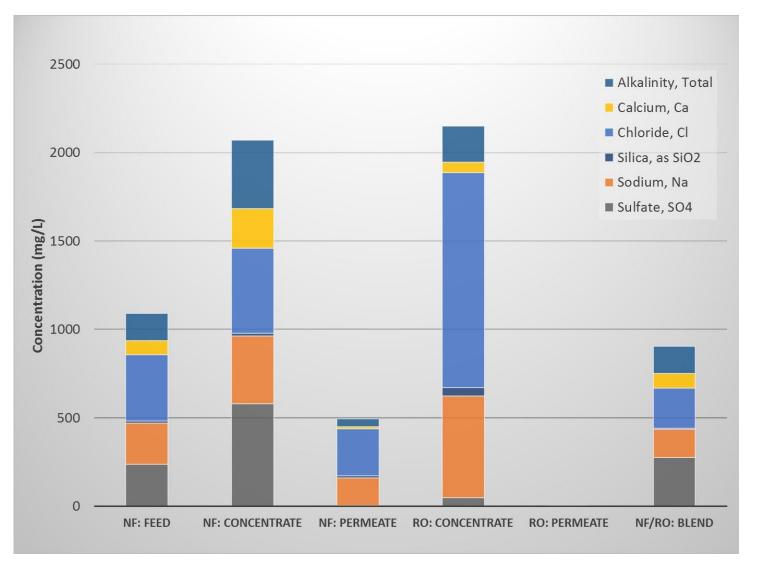
Stage 1 Specific Flux

Nanofiltration



Reverse Osmosis

Stage 1 Water Quality

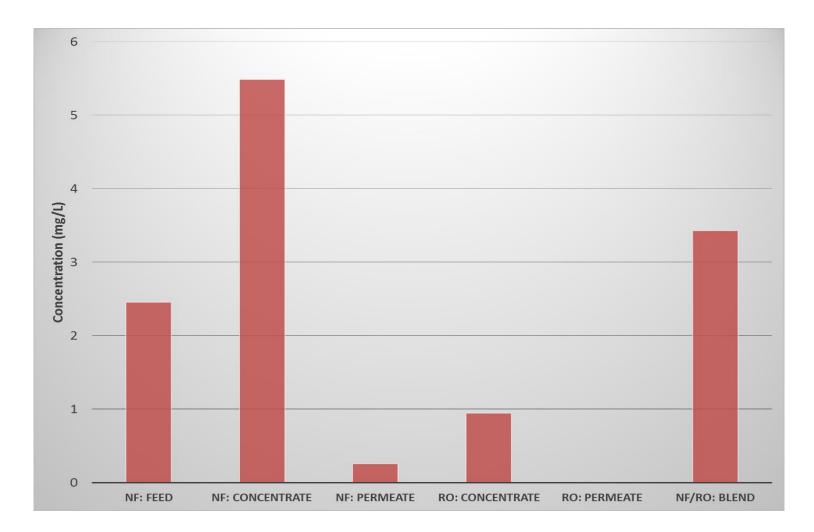


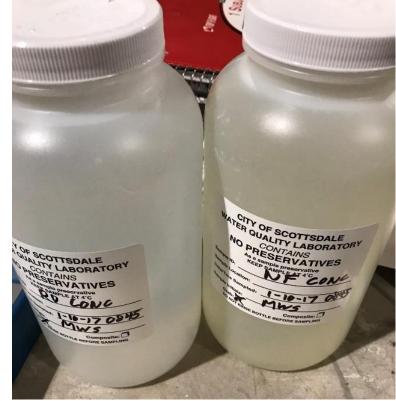
- Average TDS reduction 20%
- Good recovery of
 - Calcium 90%,
 - Sulfate >99%
 - Alkalinity 84%

Salt reduction

- Chloride 48%
- Sodium 41%

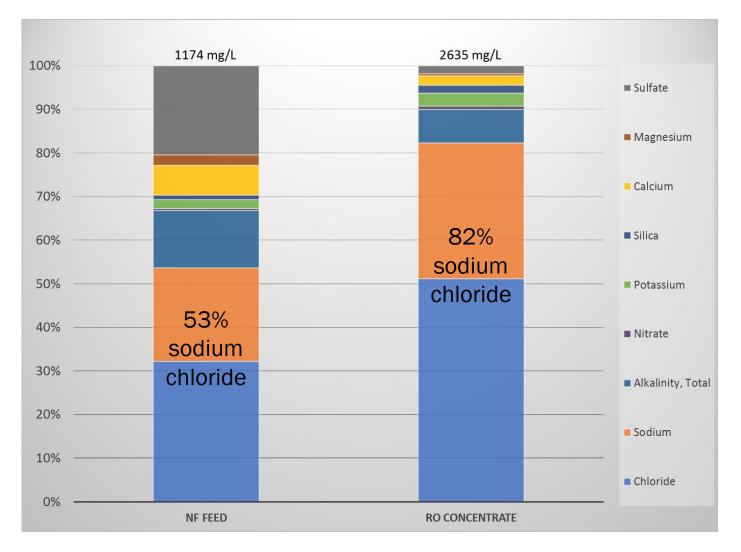
Stage 1 Water Quality (TOC)





NF concentrate clearly has higher color than RO concentrate

Stage 1



- Increase of sodium chloride percentage of TDS demonstrates selective removal
- Sulfate, calcium, magnesium make up <5% of RO concentrate vs. 30% of Feed

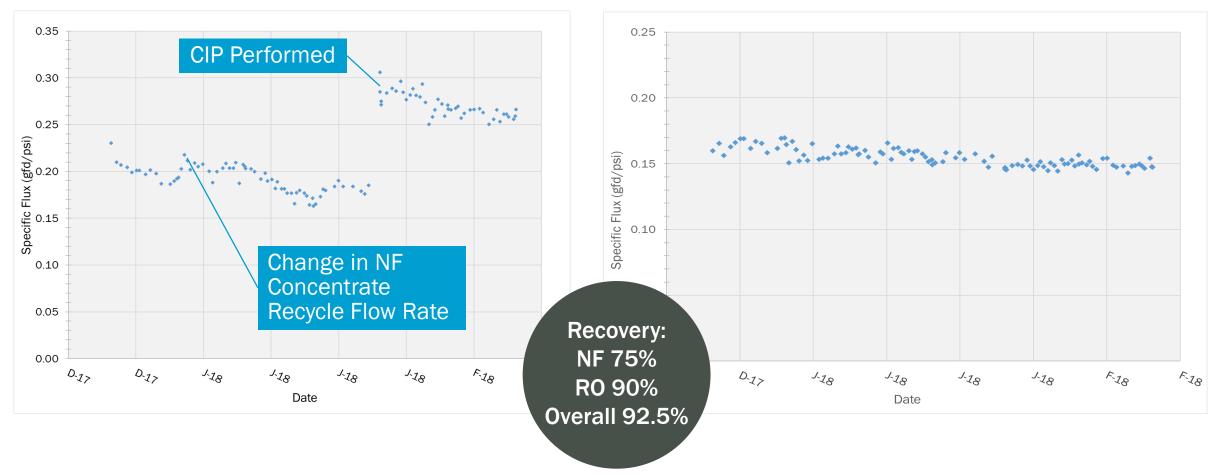
High Recovery

Stage 2 Test



Stage 2 Specific Flux

Nanofiltration



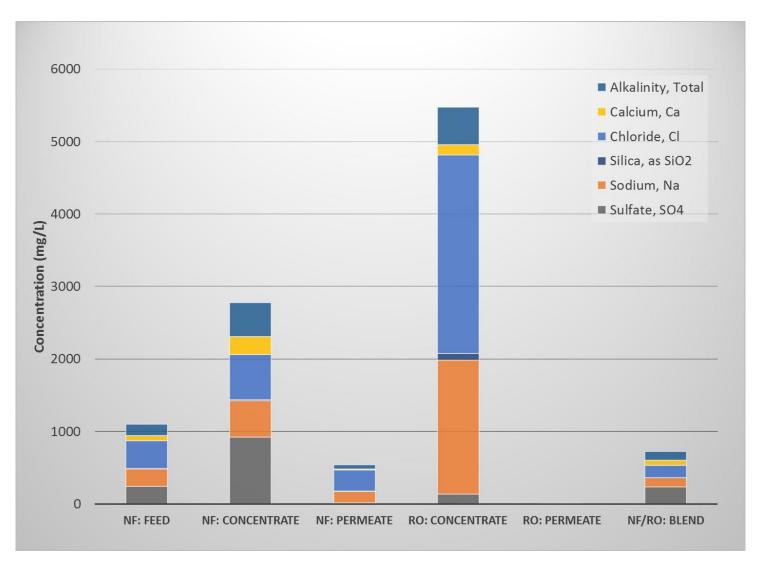
Reverse Osmosis

Stage 2



- Stage 2 NF fouling appeared to be mostly particulate fouling
- Began with 5 micron cartridge filter
- Approximately one month of operation
- Switched to 1 micron filter

Stage 2 Water Quality

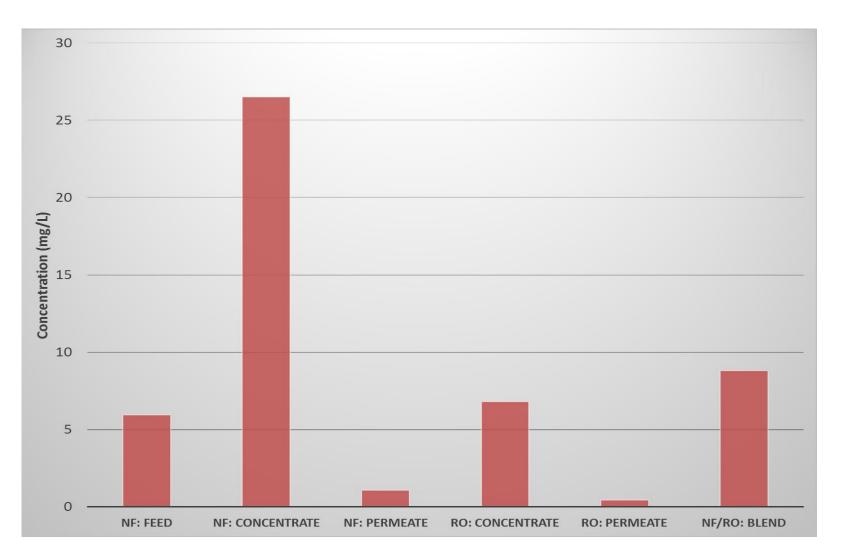


 Average TDS reduction 35%; inline with projection from NF membrane selection

Good recovery of

- Calcium 94%,
- Sulfate 99%
- Alkalinity 76%
- Salt reduction
 - Chloride 56%
 - Sodium 49%

Stage 2 Water Quality (TOC)



Data from a single sample. Feed TOC about 2x Stage 1 Detected some passage of TOC through NF membrane.

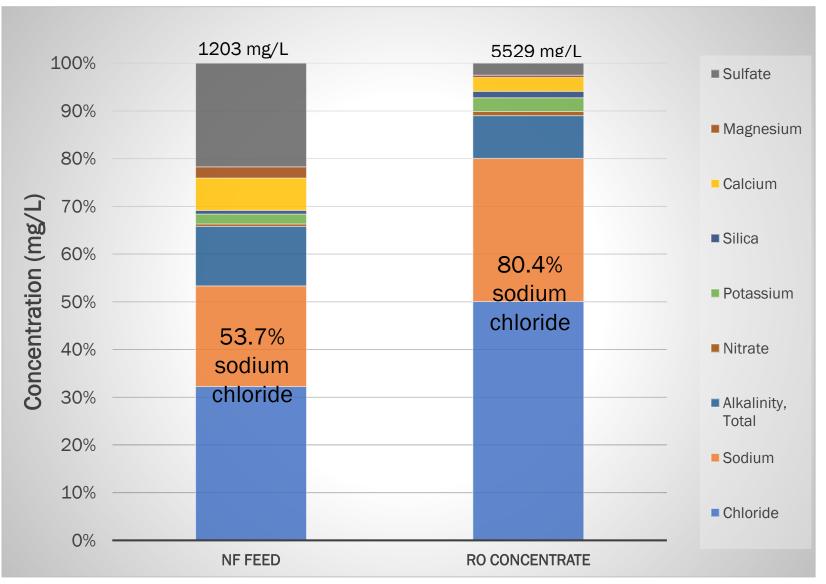
Stage 2

| UV Adsorbance, cm ⁻¹ | | | | |
|---------------------------------|--------------|--|--|--|
| Feed | 0.148 | | | |
| NF Concentrate | 0.527 | | | |
| NF Permeate | 0.020 | | | |
| RO Concentrate | 0.125 | | | |
| RO Permeate | Not Detected | | | |
| Blended Product | 0.150 | | | |

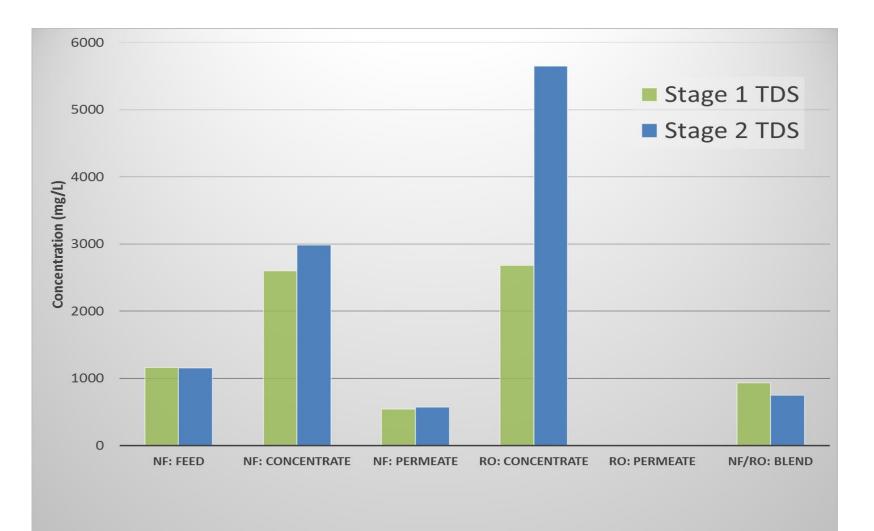


Stage 2

- Lower fraction of hardness, sulfate and alkalinity will benefit high recovery or ZLD processes
- Sulfate, calcium, magnesium make up 5% of RO concentrate vs. 30% of Feed



Water Quality Comparison (TDS)



Higher RO recovery on Stage 2 improves blended product water quality

Energy and Chemical Consumption

- Water Campus RO operating 10-20% under design during test period (25-40% less energy required)
- Pilot energy use includes recovery of NF recycle hydraulic energy
- Pilot uses no acid; RO uses approximately 42.5 lb/mg

| | Units | Water Campus RO | Stage 1 | Stage 2 |
|----------------------------|----------|-----------------|-----------|---------|
| System Recovery | | 85% | 86% | 92.5% |
| Average Energy Usage | Kwh/kgal | 0.76 - 1.16 | 1.26-1.38 | 1.44 |
| Average Anti-scalant usage | Lb/kgal | 6.9 | 3.5 | 8.6 |
| Acid usage | Lb/mg | 42.5 | 0 | 0 |

This Approach Benefits Different Concentrate Management Strategies

| | Reduced Salt Load | Reduced Volume | Reduced Chemical Consumption | Reduced Energy | Reduced Maintenance |
|---|----------------------|-------------------|------------------------------------|-------------------|------------------------|
| Disposal to sewer or interceptor | \checkmark | \checkmark | | | |
| Evaporation ponds | | \checkmark | | | |
| Thermal/Mechanical Evaporation | | \checkmark | \checkmark | \checkmark | \checkmark |
| High Recovery Processes (HERO, CCD, etc) | | \checkmark | \checkmark | \checkmark | \checkmark |
| Zero Liquid Discharge | | \checkmark | \checkmark | \checkmark | \checkmark |
| Salt recovery | | \checkmark | \checkmark | \checkmark | \checkmark |

Summary

- Selective removal of sodium chloride is possible; addresses problems with water softener discharges
- Significant reduction in concentrate volume possible with little increase in capital and operating cost
 - <10% more membrane area
 - Slightly higher energy consumption
 - Lower chemical consumption

Questions?